BREAKOUT TANK INSPECTION FORM

A completed **Standard Inspection Report** is to be submitted to the Director within 60 days from completion of the inspection. A **Post Inspection Memorandum (PIM)** is to be completed and submitted to the Director within 30 days from the completion of the inspection, or series of inspections, and is to be filed as part of the **Standard Inspection Report.**

Inspection Report	Post Inspection Memorandum	
Inspector/Submit Date: Al Jones / October 28, 2010	**Chief Eng/Review Date:**	Joe Subsits 11/2/2010
	Peer Review/Date:	
	Director Approval/Date:	

POST INSPECTION MEMORANDUM (PIM)

Name of Operator: ConocoPhillips Pipe Line Company	**OPID #:** 31684
Name of Unit(s): Yellowstone Pipe Line Company / Spokane & Moses Lake Districts	**Unit #(s):** 515
Records Location: Spokane, WA	**Activity #**
Unit Type & Commodity: Pipeline & Terminal / Refined Products	
Inspection Type: Standard	**Inspection Date(s):** Oct 12-15, 2010
PHMSA Representative(s): Al Jones / WUTC	**AFO Days:** 4

Summary:

Breakout tanks inspected at the following facilities:

- Spokane Terminal (Parkwater) - 12 tanks
- North Spokane Terminal – 9 tanks
- Fairchild Delivery Station – 2 tanks (idled)
- Geiger Delivery Station – 2 tanks (idled)
- Moses Lake Terminal – 1 tank

Findings:

There were no probable violations. Since the last inspection two tanks completed internal and external inspection in accord with API 653. All the recommendation contained in the reports was implemented by the operator. No deficiencies were found during the field inspection.

Company System Maps (copies for Region Files): **Located at the Spokane Office**

Validate SMART Data (components, miles, etc): ☐ **Acquisition(s), Sale or New Construction** (submit SMART update): ☐

Validate Additional Requirements Resulting From Waiver(s) or Special Permit(s):

Name of Operator:	ConocoPhillips Pipe Line Company		
OP ID No. [1]	31684	**Unit ID No.** [1] **515**	
HQ Address:		**System/Unit Name & Address:** [1]	
ConocoPhillips Pipe Line Company 600 Dairy Ashford Road Houston, TX 77252-2197		Yellowstone Pipe Line Company 6317 E. Sharp Ave. Spokane, WA 99211	
Co. Official:	Brian Coffman, Manager Pipeline	**Activity Record ID #:**	
Phone No.:	281-293-2338	**Phone No.:**	509-534-0686
Fax No.:		**Fax No.:**	
Emergency Phone No.:	877-267-2290	**Emergency Phone No.:**	877-267-2290

Persons Interviewed	Title	Phone No.
Chris Church	Facility Manager	507-220-2594
Larry Ferguson	Corrosion Control Specialist	406-431-0138
Mike Donally	DOT Coordinator	406-855-6913

PHMSA Representative(s) [1] **Al Jones / WUTC**	**Inspection Date(s)** [1] **Oct 12-15, 2010**

Company System Maps (Copies for Region Files):

Comments:

All breakout tanks were inspected and appeared to be in good condition. Since the last inspection two tanks completed internal and external inspection in accord with API 653. All the recommendation contained in the reports was implemented by the operator. No deficiencies were found during the field inspection.

For hazardous liquid operators, the attached evaluation form may be supplemented with PHMSA Form 3 and 49 CFR 195 during PHMSA inspections.

[1] Information not required if included on page 1.

		Design and New Construction of Aboveground Breakout Tanks	S	U	N/A	N/C
.132	(a)	Each aboveground breakout tank must be designed and constructed to withstand the internal pressure produced by the hazardous liquid to be stored therein and any anticipated external loads.	X			
	(b)	After Oct. 2, 2000 compliance with paragraph (a) above requires:				
		(1) Shop-fabricated, vertical, cylindrical, closed top, welded steel tanks with nominal capacities of 90 to 750 barrels and with internal vapor space pressures that are approximately atmospheric must be designed and constructed in accordance with API Specification 12F.			X_1	
		(2) Welded, low-pressure (i.e., internal vapor space pressure not greater than 15 psig) carbon steel tanks that have wall shapes that can be generated by a single vertical axis of revolution must be designed and constructed in accordance with API Standard 620.			X_2	
		(3) Vertical, cylindrical, welded steel tanks with internal pressures at the tank top approximating atmospheric pressures (i.e., internal vapor space pressures not greater than 2.5 psig, or not greater than the pressure developed by the weight of the tank roof) must be designed and constructed in accordance with API Standard 650.	X			
		(4) High pressure steel tanks (i.e., internal gas or vapor space pressures greater than 15 psig) with a nominal capacity of 2000 gallons or more of LPG must be designed and constructed in accordance with API Standard 2510.			X_3	

Comments:
All breakout tanks are designed to API Standard **650** or its predecessor Standard **12C**.

		Tank Repairs, Alterations, and Reconstruction Procedures	S	U	N/A	N/C
.205	(a)	Aboveground breakout tanks repaired, altered, or reconstructed and returned to service must be capable of withstanding the internal pressure produced by the hazardous liquid to be stored therein and any anticipated external loads. *The repair/alteration history includes all data accumulated on a tank from the time of its construction with regard to repairs, alterations, replacements, and service changes (recorded with service conditions such as stored product temperature and pressure). These records should include the results of any experiences with coatings and linings.*	X			
	(b)	After Oct. 2, 2000 compliance with paragraph (a) above requires:				
		(1) Tanks designed for approximately atmospheric pressure, constructed of carbon and low alloy steel, welded or riveted, and non-refrigerated built to **API Standard 650 (Welded Steel Tanks for Oil Storage)** must be repaired, altered, or reconstructed according to API Standard 653. *The basis for repairs and alterations shall be an API Standard 650 equivalence*	X			
		(2) Tanks built to API Specification 12F (Specification for Shop Welded Tanks for Storage of Production Liquids) or API Standard 620 (Design, Construction, Large, Welded, Low-Pressure Storage Tanks), the repair, alteration, and reconstruction must be in accordance with the design, welding, examination, and material requirements of those respective standards. Tanks built to API 620 may be modified by the design, welding examination and testing provisions of API 653 in proper conformance with the stresses, joint efficiencies, material and other provisions in API standard 620.	X			
		(3) For high pressure tanks built to API Standards 2510 (Design and Construction of LPG Installations), repaired, altered, or reconstructed will be in accordance with API 510 (Pressure Vessel Inspection Code).			X_4	

Comments:
Footnotes #1-#4: All breakout tanks are designed to API Standard **650** or its predecessor Standard **12C**.

		Impoundment, Protection Against Entry, Relief, and Venting Procedures	S	U	N/A	N/C
.264	(a)	A means must be provided for containing hazardous liquids in the event of spillage or failure of an aboveground breakout tank. Containment and impoundment are effective means of controlling environmental releases and fires.	X			
	(b)	(1) For tanks built to **API Specification 12F (Specification for Shop Welded Tanks for Storage of Production Liquids) , API Standard 620 (Design, Construction, Large, Welded, Low-Pressure Storage Tanks)**, and others (such as **API Standard 650** or its predecessor Standard **12C**), the installation of impoundment must be in accordance with the following sections of **NFPA 30 (Flammable and Combustible Liquids Code):**				
		(i) Impoundment around a breakout tank must be installed in accordance with Section 3.2.3.2; and	X			
		(ii) Impoundment by drainage to a remote impounding area must be installed in accordance with Section 4.3.2.3.1.	X			
		(2) For tanks built to **API Standard 2510**, the installation of impoundment must be in accordance with Section 5 or 11 of **API Standard 2510. (Design and Construction of LPG Installations):** *Refer to Section 5 API Standard 2510 - Siting Requirements and Spill Containment*			X_5	
	(c)	Aboveground breakout tank areas must be adequately protected against unauthorized entry.	X			
	(d)	Normal/emergency relief venting must be provided for each atmospheric pressure breakout tank. Each low-pressure and high-pressure breakout tank must have pressure/vacuum-relieving devices.	X			
	(e)	For normal/emergency relief venting and pressure/vacuum-relieving devices installed on aboveground breakout tanks after October 2, 2000, compliance with paragraph (d) of this section requires the following for the tanks specified:				
		(1) Normal/emergency relief venting installed on atmospheric pressure tanks built to **API Specification 12F (Specification for Shop Welded Tanks for Storage of Production Liquids)** must be in accordance with Section 4, and Appendices B and C, of **API Specification 12F (Specification for Shop Welded Tanks for Storage of Production Liquids) .**			X_6	
		(2) Normal/emergency relief venting installed on atmospheric pressure tanks (such as those **built to API Standard 650** or its predecessor **Standard 12C**) must be in accordance with **API Standard 2000. (Venting Atmospheric and Low-Pressure Storage Tanks Nonrefrigerated and Refrigerated)**	X			
		(3) Pressure-relieving and emergency vacuum-relieving devices installed on low pressure tanks built to **API Standard 620 (Design, Construction, Large, Welded, Low-Pressure Storage Tanks)** must be in accordance with Section 9 of API Standard 620 and its references to the normal and emergency venting requirements in API Standard 2000.			X_7	
		(4) Pressure and vacuum-relieving devices installed on high pressure tanks built to **API Standard 2510 (Design and Construction of LPG Installations):** must be in accordance with Sections 7 or 11 of API Standard 2510.			X_8	

Comments:
Footnotes #5-#8: All breakout tanks are designed to API Standard **650** or its predecessor Standard **12C**.

		Pressure Test Procedures/Pressure Testing Aboveground Breakout Tanks	S	U	N/A	N/C
.307	(a)	Aboveground breakout tanks built to **API Specification 12F (Specification for Shop Welded Tanks for Storage of Production Liquids)** and first placed in service after October 2, 2000, pneumatic testing must be in accordance with section 5.3 of API Specification 12F.			X_9	
	(b)	Aboveground breakout tanks built to **API Standard 620 (Design, Construction, Large Welded Low Pressure Storage Tanks)** and first placed in service after October 2, 2000, hydrostatic and pneumatic testing must be in accordance with section 7.18 of API Standard 620.			X_{10}	
	(c)	Aboveground breakout tanks built to **API Standard 650 (Welded Steel Tanks For Oil Storage)** and first placed in service after October 2, 2000, hydrostatic and pneumatic testing must be in accordance with section 5.3 of API Standard 650.	X			
	(d)	Aboveground atmospheric pressure breakout tanks constructed of carbon and low alloy steel, welded or riveted, and non-refrigerated and tanks built to **API Standard 650 Welded Steel Tanks For Oil Storage)** or its predecessor **Standard 12C** that are returned to service after October 2, 2000, the necessity for the hydrostatic testing of repair, alteration, and reconstruction is covered in section 12.3 of API Standard 653.	X			

Pressure Test Procedures/Pressure Testing Aboveground Breakout Tanks			S	U	N/A	N/C
	(e)	Aboveground breakout tanks **built to API Standard 2510 (Design and Construction of LPG Installations)** and first placed in service after October 2, 2000, pressure testing must be in accordance with ASME Boiler and Pressure Vessel Code, Section VIII, Div.1 or 2.			X_{11}	
.310	(a)	A record must be made of each pressure test required by this subpart, and the record of the latest test must be retained as long as the facility tested is in use.			X_{12}	
	(b)	The record required by paragraph (a) of this section must include: (1) The pressure recording charts; (2) Test instrument calibration data; (3) The name of the operator, the name of the person responsible for making the test, and the name of the test company used, if any; (4) The date and time of the test; (5) The minimum test pressure; (6) The test medium; (7) A description of the facility tested and the test apparatus; (8) An explanation of any pressure discontinuities, including test failures, that appear on the pressure recording charts; (9) Where elevation differences in the section under test exceed 100 feet (30 meters), a profile of the pipeline that shows the elevation and test sites over the entire length of the test section; and (10) Temperature of the test medium or pipe during the test period.			X_{13}	

Comments:
Footnotes #9-#13: All breakout tanks are designed to API Standard **650** or its predecessor Standard **12C**.

BREAKOUT TANK PROCEDURES			S	U	N/A	N/C
.402(c)(3)	.404(a)	Operator shall maintain current maps and records of its pipeline systems that include at least the following information; (1) Location and identification of (i) breakout tanks.	X			
	.405(a)	Provide protection against ignitions arising out of static electricity, lightning, and stray currents IAW **API Recommended Practice 2003 (Protection Against Ignitions Arising Out of Static, Lightning, and Stray Currents)**. ***(Refer to Subsection 4.5, Subsection 4.6, Subsection 5.4 , Subsection 5.5, and Subsection 6.3 of API RP 2003)***	X			
	.405(b)	Review, consider, and incorporate into operator's procedure manual, the potentially hazardous conditions, safety practices and procedures associated with access/egress onto floating roofs IAW **API 2026 (Safe Access/Egress Involving Floating Roofs of Storage Tanks In Petroleum Service)**.	X			
	.422	Repairs shall be made in a safe manner and made so as to prevent damage to persons or property.	X			
	.428(a)	Inspect and test each pressure limiting device, relief valve, pressure regulator, or other pressure control equipment (annually/NTE 15 mo), except as provided in paragraph (b) of this section.	X			
	.428(b)	In the case of relief valves on pressure breakout tanks containing **HVLs**, operator shall test each valve at intervals not exceeding 5 years.			X_{14}	
	.428(c)	Aboveground breakout tanks • constructed or significantly altered according to section 5.1.2 of **API Standard 2510 (Design and Construction of LPG Installations)** after October 2, 2000 must have an overfill protection system according to 5.1.2 of API Standard 2510. • **if (600 gallons or more)** constructed or significantly altered after October 2, 2000, must have overfill protection according to **API Recommended Practice 2350 (Overfill Protection for Storage Tanks in a Petroleum Facility)**. **For <u>Unattended Facilities</u> (defined in API RP 2350, paragraph 1.3.1) Section 2, for <u>Attended Facilities</u> (defined in API RP 2350, paragraph 1.3.1) Section 3, and for all facilities, Transfer Procedures need to be per Section 4.**			X_{15}	
	.428(d)	After October 2, 2000, paragraphs (a) and (b) of §195.428 also applies for the inspection and testing of pressure control equipment and to the testing of overfill protection systems.			X_{16}	

		BREAKOUT TANK PROCEDURES	S	U	N/A	N/C
	.430	Each operator shall maintain adequate firefighting equipment at each pump station and breakout tank area. The equipment must be– (a) In proper operating condition at all times; (b) Plainly marked so that its identity as firefighting equipment is clear; and (c) Located so that it is easily accessible during a fire.	X			
	.432(b)	Each operator shall inspect the physical integrity of in-service atmospheric and low-pressure steel aboveground breakout tanks according to **section 6 of API Standard 653.** However, if structural conditions prevent access to the tank bottom, the bottom integrity may be assessed according to a plan included in the operations and maintenance manual under **§195.402(c)(3).**			X_{17}	
		-Owner/operator visual, external condition inspection interval not to exceed **one month** (more frequent inspections may be needed based on conditions at particular sites)	X			
		-External inspection, visual, by an Authorized Inspector at least every **five years** or at the quarter corrosion rate life of the shell, whichever is less. -External ultrasonic thickness measurement of the shell based on the corrosion rate. If the corrosion rate is not known, the maximum interval shall be **five years**.	X			
		Are corrosion rate-based internal inspection intervals established in accordance with API 653, and in no case exceed **20 years**?	X			
		If tank bottom upper or lower side corrosion rate is unknown, the Out of Service inspection interval shall not exceed **10 years**.	X			
	.432(c)	Each operator shall inspect the physical integrity of in-service steel aboveground breakout tanks built to **API Standard 2510** according to **section 6 of API 510.** Amt. 195-86 Pub. 06/09/06 eff 07/10/06.			X_{18}	
	.432(d)	The intervals of inspection specified by documents referenced in paragraphs (b) and (c) of this section begin on **May 3, 1999**, or on the operator's last recorded date of the inspection, whichever is earlier.	X			
	.434	Maintain signs visible to the public around each breakout tank area. Each sign must contain the name of the operator and a telephone number (including area code) where the operator can be reached at all times.	X			
	.436	Operator shall provide protection for each breakout tank area and other exposed facility (such as scraper traps) from vandalism and unauthorized entry.	X			
	.438	Operator shall prohibit smoking and open flames in each breakout tank area where there is a possibility of the leakage of a flammable hazardous liquid or of the presence of flammable vapors.	X			

Comments:
Footnotes:
#14 & #16: No HVL Tanks.
#15: All breakout tanks are designed to API Standard **650** or its predecessor Standard **12C**.
#17: All double bottom tanks.

		Corrosion Control Procedures	S	U	N/A	N/C
.402(c)(3)	**.563(d)**	Breakout tank areas, bare pipelines, and buried pumping station piping must have cathodic protection in places where previous editions of this part required cathodic protection as a result of electrical inspections.	X			
	.565	**Breakout Tank CP installation** Does operator install (after 10/2/00) required cathodic protection systems to protect above ground breakout tanks over 500 bbl capacity, in accordance with API RP 651?	X			
	.571	**Cathodic Protection (CP) Acceptance Criteria** CP levels must comply with NACE Standard RP0169-96 (paragraphs 6.2 and 6.3)	X			
	.573(d)	**Breakout Tank CP inspections** Cathodic protection systems used to protect breakout tanks must be inspected in accordance with API 651.	X			
	11.3.2	**Cathodic Protection Surveys** – Annual CP surveys are required. Surveys may include one or more of the following:				
		1. Structure to soil potential.	X			
		2. Anode current.	X			
		3. Native structure to soil potentials	X			
		4. Structure-to-structure potential	X			
		5. Piping-to-tank isolation if protected separately.	X			
		6. Structure-to-soil potential on adjacent structures.	X			

		Corrosion Control Procedures	S	U	N/A	N/C
		7. Continuity of structures if protected as a single structure.	X			
		8. Rectifier DC volts, DC amps, efficiency, and tap settings.	X			
		Rectifier Inspections:				
		- Every 2 months. – (Inspections should include a check for electrical shorts, ground connections, meter accuracy, and circuit resistance).	X			
	11.3.3.4	**Tank Bottoms** – Tank bottom should be examined for evidence of corrosion whenever access to the bottom is possible. (During repairs, modifications, during API653 inspections) Examinations may be done by coupon cutouts or nondestructive methods.	X			
	.577(a)	**Interference Currents** For breakout tanks exposed to stray currents, is there a program to minimize the detrimental effects?	X			
	.579(d)	**Breakout tank – internal corrosion mitigation** After October 2, 2000, tank bottom linings installed in tanks built to **API 12F (Specification for Shop Welded Tanks for Storage of Production Liquids), API 620 (Design, Construction, Large, Welded, Low-Pressure Storage Tanks), API 650 (Welded Steel Tanks for Oil Storage), or its predecessor 12C** must be installed in accordance with API RP 652.	X			
	.581(c)	**Atmospheric Corrosion Protection** Except for soil-to-air interfaces, atmospheric corrosion protection is not required where it is demonstrated by test, investigation, or similar environmental experience; that corrosion will – (1) Only be a light surface oxide; or (2) Not affect the safe operation of the pipeline before the next scheduled inspection.	X			
	.583(a)	**Atmospheric Corrosion Monitoring** Inspect each pipeline that is exposed to the atmosphere for evidence of atmospheric corrosion at least once every 3 calendar years, but with intervals not exceeding 39 months.	X			
	.583(c)	If you find atmospheric corrosion during an inspection, you must provide protection against the corrosion as required by §195.581.	X			

Comments:
All breakout tanks are designed to API Standard **650** or its predecessor Standard **12C**.

	FIELD REVIEW	S	U	N/A	N/C
.258(a)	Is each valve installed in a location that is accessible to authorized employees and protected from damage or tampering?	X			
.260(b)	A valve must be installed on each line entering or leaving a breakout storage tank area in a manner that permits isolation of the tank area from other facilities.	X			
.264	Impoundment areas adequate, dikes not eroded, and dike drains operational.	X			
.428	Pressure Limiting Devices, relief valve, pressure regulator, overfill protection systems.	X			
.430	Each operator shall maintain adequate firefighting equipment at each breakout tank area that is: • In proper operating condition, • Plainly marked, and • Located to be readily accessible	X			
.434	Signs visible to the public around each breakout tank area that contains the name of the operator and a telephone number (including area code) where the operator can be reached at all times.	X			
.436	Protection for each breakout tank area from vandalism and unauthorized entry.	X			
.438	Prohibition of smoking and open flames in breakout tank areas	X			
.565	Cathodic Protection System Facilities	X			
.581	Atmospheric Corrosion (piping, tanks, soil/air interfaces, splash zones)	X			
.501-.509	**Operator Qualification** - Use PHMSA Form 15 Operator Qualification Field Inspection Protocol	X			

Comments:

Comments:

Breakout Tank Field Review (Complete one page for each tank or tank impound area inspected)						
.432	**Tank Number(s)**		**S**	**U**	**N/A**	**N/C**
	General Site Conditions	a. Runoff rainwater from the shell drains away from tank, and site drainage away from tank.	X			
		b. No vegetation against tanks, no flammable materials, trash.	X			
		c. No voids under tank/tank foundations, or settlement around perimeter of tank.	X			
	Tank Foundation, Bottom Shell	a. Concrete (no broken concrete, spalling, or cracks).	X			
		b. Plate and weld in bottom angle area (No thinning or corrosion).	X			
		c. Integrity of the bottom-to-foundation seal, if present.	X			
		d. No signs of bottom leakage.	X			
	External Shell	a. Exterior coating (No paint failure, pitting, or corrosion).	X			
		b. Rivet or seam leakage.			X_{19}	
		c. No cracks or signs of leakage on weld joints at nozzles, manways, and reinforcing plates.	X			
		d. No shell deformation.	X			
		e. No shell plate dimpling around nozzles, caused by excessive pipe deflection.	X			
	Tank Piping and Manifolds	a. No manifold piping, flange, or valve leakage.	X			
		b. Anchored piping (check that it would not cause tank shell bottom connection damage during earth movement).	X			
		c. Adequate thermal pressure relief of piping to the tank.	X			
		d. Temperature indicators are accurate and undamaged.	X			
	Shell-Mounted Sample Station	a. Sample line and return-to-tank line valves, seals, and drains function properly.	X			
		b. Circulation pump has no signs of leaks or operating problems.			X_{20}	
	Mixer	a. Mounting flange is properly supported.	X			
		b. No signs of leaks or operating problems.	X			
	Gauging System(s)	a. Verify proper operating condition	X			
		b. Evidence of operating problems	X			
	Inspection Recommendation(s) Follow-up	a. Have recommended actions from inspection reports been taken?	X			
		b. Have repairs identified by required inspections been made?	X			

Comments:
Footnotes:
#19: All welded tank seams.
#20: No shell-mounted circulation pumps.

	RECORDS REVIEW	S	U	N/A	N/C
.132	Design and Construction of aboveground breakout tanks	X			
.205(b)	Tank alteration and reconstruction records. For tanks repaired after 10/2/2000, records reflecting compliance with the referenced API standards.	X			
.264	Impoundment determination records. For tanks constructed after October 2, 2000, records reflecting compliance with the referenced API/NFPA standards.	X			
.264(d)	Record of calculations for normal/relief vents and pressure/vacuum vents.	X			
.310	Hydrostatic/pneumatic testing records for above ground breakout tanks for tanks first placed in service after 10/2/2000.			X_{21}	
.404(a)	Maps and records of location and identification of breakout tanks	X			
.405(a)	API RP 2003 (if not followed by operator, must have a documented basis)	X			
.405(b)	Review applicable hazards in API RP 2026 for inclusion in the procedure manual	X			
.428	Testing of overpressure safety devices and overfill protection systems	X			
.432	Inspection of in-service breakout tanks (in accordance with applicable API Standard)				
	Monthly inspection reports	X			
	Annual inspection report(s)	X			
	In-service inspection report(s), including next inspection interval calculation	X			
	Out-of-service inspection report(s), including next inspection interval calculation	X			
	Follow-up actions from inspection findings (repairs, fill level height adjustments, other recommendations from inspection report).	X			
.573	External corrosion control monitoring records in accordance with API RP 651	X			
	Rectifiers (6 times per calendar year, not to exceed 2 ½ month intervals)	X			
	Electrical isolation and or bonds			X_{22}	
	Structure to Soil potentials, annual surveys	X			
.579	Tank bottom linings in accordance with API RP 652, if installed after October 2, 2000	X			
.581	Atmospheric corrosion monitoring (every 3 years not to exceed 39 months)				
.589	Maintain current records or maps to show the location of cathodic protection and monitoring facilities, including galvanic anodes, installed after January 29, 2002, and neighboring structures bonded to cathodic protection systems.	X			

Comments:
Footnotes:
#21: No tanks are constructed since 10/2/2000.
#22: No isolation bonds exist with other structures.

TANK DATA

(See Note Below for * Items)		1	2	3	4	5	6
	FACILITY NAME(S):	Spokane (Parkwater)	Spokane (Parkwater)	Spokane (Parkwater)	Spokane (Parkwater)	Spokane (Parkwater)	Spokane (Parkwater)
*(A)	PRODUCT	R	R	R	R	out of service	R
(B)	TANK #	70	71	72	73	74	75
(C)	CONSTRUCTION YEAR and API STANDARD	1953	1953	1953	1953	1953	1995
*(D)	CONSTRUCTION TYPE	W	W	W	W	W	W
(E)	CAPACITY (BBL)	29,612	28,741	50,927	28,998	2,030	8,000
(F)	LINING? (Y/N)	Y	Y	N	Y	N	Y
(G)	LINING TYPE?	Epoxy	Epoxy	Epoxy	Epoxy	Epoxy	Epoxy
(H)	TANK HT.(FT)	40	40	40	40	20	40
(I)	MAX. FILL HT. (FT)	39.3	37	36.6	39.4	19	36.2
(J)	DIA (FT)	73.3	73.3	100	73.3	40	120
*(K)	ROOF TYPE	F	EF	IF	F	F	IF
*(L)	VOLUMETRIC ALARM(S)	HH	HH	HH	HH	HH	HH
(M)	DIKE VOLUME (BBL)	153,964	153,964	153,964	153,964	2,738	153,964
*(N)	DATE LAST INTERNAL INSPECTION	6/28/2006	6/23/2006	12/14/2005	12/14/2005	7/17/1999	7/7/2005
*(O)	OUT OF SERVICE REPAIR OR OTHER MAJOR REPAIR	1/30/2007 new floor	1/30/2007 new floor	12/14/1995 new seals	8/16/2000 new floor	out of service	2/13/2007 repair bottom coating
(P)	DATE API 653 APPLIED	6/28/2006	2/23/2006	10/26/4995	12/14/2005	out of service	7/7/2005
*(Q)	CP TYPE & ANODE TYPE	R	R	R	R	R	R
*(R)	C P MONITORING	Yes	Yes	Yes	Yes	Yes	Yes
(S)	DUE DATE FOR NEXT INTERNAL INSPECTION?	6/28/2016	6/23/2016	3/24/2020	5/20/2020	out of service	6/15/2015
(T)	INTERNAL INSPECTION INTERVAL? (YEARS)	10 years	10 years	14 years	10 years	out of service	10 years
*(U)	INTERNAL INSPECTION INTERVAL BASIS?	New floor, unknown corrosion rate.	New floor, unknown corrosion rate.	New floor, unknown corrosion rate.	New floor, unknown corrosion rate.	out of service	Close-up seal inspection
(V)	DUE DATE FOR NEXT EXTERNAL INSPECTION?	6/28/2011	6/23/2011	12/14/2015	12/14/2015	out of service	12/1/2016
*(W)	EXTERNAL INSPECTION INTERVAL BASIS?	M	M	M	M	out of service	M
(X)	DUE DATE FOR NEXT U. T. INSPECTION?	6/28/2011	6/23/2011	12/14/2015	12/14/2015	out of service	12/1/2016
(Y)	SHELL U.T. INSPECTION INTERVAL	5 years	5 years	5 years	5 years	out of service	5 years
*(Z)	SHELL U.T. INSPECTION INTERVAL BASIS?	M	M	M	M	out of service	M

NOTE: Enter the applicable codes below in the table above:

(A): (R) Refined; (C) Crude; (HVL) Highly Volatile Liquid; (O) Other
(D): (W) Welded; (R) Riveted; (B) Bolted; Note if Tank is Insulated
(K): (EF) External Floater; (IF) Internal Floater; (F) Fixed
(L): (H) High; (HH) High-High; (OF) Overfill; (O) Other
(N): Most Recent Date
(O): Most Recent Date
(Q): (A) Anodic; (R) Rectified (N) None - Document why not needed.
(R): (F) Fixed Reference Cells Under Floor; (S) CP Monitored at Edge of Shell
(U): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service
(W): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service
(Z): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service

Comments:
All breakout tanks are designed to API Standard **650** or its predecessor Standard **12C**.

TANK DATA

(See Note Below for * Items)		7	8	9	10	11	12
FACILITY NAME(S):		Spokane (Parkwater)	Spokane (Parkwater)	Spokane (Parkwater)	Spokane (Parkwater)	Spokane (Parkwater)	Spokane (Parkwater)
*(A)	PRODUCT	R	R	R	R	out of service	R
(B)	TANK #	80	81	82	83	84	85
(C)	CONSTRUCTION YEAR and API STANDARD	1953	1953	1953	1953	1953	1995
*(D)	CONSTRUCTION TYPE	W	W	W	W	W	W
(E)	CAPACITY (BBL)	27,844	18,273	20,000	20,000	18,271	27,978
(F)	LINING? (Y/N)	Y	Y	N	Y	N	Y
(G)	LINING TYPE?	Epoxy	Epoxy	Epoxy	Epoxy	Epoxy	Epoxy
(H)	TANK HT.(FT)	40	40	40	40	40	40
(I)	MAX. FILL HT. (FT)	38	36.5	39.1	38	36	37.4
(J)	DIA (FT)	73.3	60	60	60	60	73.3
*(K)	ROOF TYPE	IF	IF	F	IF	IF	EF
*(L)	VOLUMETRIC ALARM(S)	HH	HH	HH	HH	HH	HH
(M)	DIKE VOLUME (BBL)	43,577	43,577	43,577	43,577	43,577	43,577
*(N)	DATE LAST INTERNAL INSPECTION	8/22/2005	2/18/2003	4/8/2005	3/8/2004	5/1/2001	2/18/2003
*(O)	OUT OF SERVICE REPAIR OR OTHER MAJOR REPAIR	1/16/2006 new floor	3/5/2003 new floor	7/15/2005 new floor	8/16/2004 new floor	5/1/2001 new floor	8/25/2003 new floor
(P)	DATE API 653 APPLIED	8/22/2005	2/18/2003	4/8/2005	3/8/2004	5/1/2001	2/18/2003
*(Q)	CP TYPE & ANODE TYPE	R	R	R	R	R	R
*(R)	C P MONITORING	Yes	Yes	Yes	Yes	Yes	Yes
(S)	DUE DATE FOR NEXT INTERNAL INSPECTION?	8/22/2015	2/18/2013	4/8/2015	10/1/2014	9/1/2011	2/1/2013
(T)	INTERNAL INSPECTION INTERVAL? (YEARS)	10 years	10 years	10 years	10 years	10 years	10 years
*(U)	INTERNAL INSPECTION INTERVAL BASIS?	Close-up seal inspection.	Close-up seal inspection	New floor	Close-up seal inspection	Close-up seal inspection	New floor
(V)	DUE DATE FOR NEXT EXTERNAL INSPECTION?	8/22/2020	2/18/2018	4/8/2020	3/8/2019	8/23/2011	2/18/2018
*(W)	EXTERNAL INSPECTION INTERVAL BASIS?	M	M	M	M	M	M
(X)	DUE DATE FOR NEXT U. T. INSPECTION?	8/22/2015	2/18/2013	4/8/2015	3/8/2014	8/23/2011	2/18/2018
(Y)	SHELL U.T. INSPECTION INTERVAL	5 years	5 years	5 years	5 years	5 years	5 years
*(Z)	SHELL U.T. INSPECTION INTERVAL BASIS?	M	M	M	M	M	M

NOTE: Enter the applicable codes below in the table above:

(A): (R) Refined; (C) Crude; (HVL) Highly Volatile Liquid; (O) Other
(D): (W) Welded; (R) Riveted; (B) Bolted; Note if Tank is Insulated
(K): (EF) External Floater; (IF) Internal Floater; (F) Fixed
(L): (H) High; (HH) High-High; (OF) Overfill; (O) Other
(N): Most Recent Date
(O): Most Recent Date
(Q): (A) Anodic; (R) Rectified (N) None - Document why not needed.
(R): (F) Fixed Reference Cells Under Floor; (S) CP Monitored at Edge of Shell
(U): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service
(W): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service
(Z): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service

Comments:
All breakout tanks are designed to API Standard **650** or its predecessor Standard **12C**.

TANK DATA

(See Note Below for * Items)		13	14	15	16	17	18
	FACILITY NAME(S):	North Spokane	North Spokane	North Spokane	North Spokane	North Spokane	North Spokane
*(A)	PRODUCT	R	R	R	R	out of service	R
(B)	TANK #	96	97	98	99	100	101
(C)	CONSTRUCTION YEAR and API STANDARD	1959/12C	1959/12C	1959/12C	1959/12C	1959/12C	1959/12C
*(D)	CONSTRUCTION TYPE	W	W	W	W	W	W
(E)	CAPACITY (BBL)	80,784	80,000	80,000	80,000	55,000	55,000
(F)	LINING? (Y/N)	Y	Y	N	Y	N	Y
(G)	LINING TYPE?	Epoxy	Epoxy	Epoxy	Epoxy	Epoxy	Epoxy
(H)	TANK HT.(FT)	40	40	40	40	40	40
(I)	MAX. FILL HT. (FT)	37	38	36	37	37	36
(J)	DIA (FT)	120	120	120	120	100	100
*(K)	ROOF TYPE	EF	EF	EF	EF	EF	EF
*(L)	VOLUMETRIC ALARM(S)	HH	HH	HH	HH	HH	HH
(M)	DIKE VOLUME (BBL)	98,170	93,855	88,784	92,090	62,814	61,888
*(N)	DATE LAST INTERNAL INSPECTION	7/11/2003	6/25/2001	10/11/2005	8/5/2004	9/10/2002	9/14/2006
*(O)	OUT OF SERVICE REPAIR OR OTHER MAJOR REPAIR	7/11/2003 new floor	6/25/2001 new floor	10/11/2005 new floor	8/5/2004 new floor	9/10/2002 new floor	9/14/2006 new floor
(P)	DATE API 653 APPLIED	7/11/2003	6/25/2001	10/11/2005	8/5/2004	9/10/2002	9/14/2006
*(Q)	CP TYPE & ANODE TYPE	R	R	R	R	R	R
*(R)	C P MONITORING	Yes	Yes	Yes	Yes	Yes	Yes
(S)	DUE DATE FOR NEXT INTERNAL INSPECTION?	2013	2011	2015	2014	2012	2016
(T)	INTERNAL INSPECTION INTERVAL? (YEARS)	10 years	10 years	10 years	10 years	10 years	10 years
*(U)	INTERNAL INSPECTION INTERVAL BASIS?	New floor	New floor	New floor	New floor	New floor	New floor
(V)	DUE DATE FOR NEXT EXTERNAL INSPECTION?	2013	2011	2015	2014	2012	2016
*(W)	EXTERNAL INSPECTION INTERVAL BASIS?	M	M	M	M	M	M
(X)	DUE DATE FOR NEXT U. T. INSPECTION?	2013	2011	2015	2014	2012	2016
(Y)	SHELL U.T. INSPECTION INTERVAL	5 years	5 years	5 years	5 years	5 years	5 years
*(Z)	SHELL U.T. INSPECTION INTERVAL BASIS?	M	M	M	M	M	M

NOTE: Enter the applicable codes below in the table above:

(A): (R) Refined; (C) Crude; (HVL) Highly Volatile Liquid; (O) Other
(D): (W) Welded; (R) Riveted; (B) Bolted; Note if Tank is Insulated
(K): (EF) External Floater; (IF) Internal Floater; (F) Fixed
(L): (H) High; (HH) High-High; (OF) Overfill; (O) Other
(N): Most Recent Date
(O): Most Recent Date
(Q): (A) Anodic; (R) Rectified (N) None - Document why not needed.
(R): (F) Fixed Reference Cells Under Floor; (S) CP Monitored at Edge of Shell
(U): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service
(W): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service
(Z): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service

Comments:
All breakout tanks are designed to API Standard **650** or its predecessor Standard **12C**.

TANK DATA

(See Note Below for * Items)		19	20	21	22		
	FACILITY NAME(S):	North Spokane	North Spokane	North Spokane	Moses Lake		
*(A)	PRODUCT	R	R	R	R		
(B)	TANK #	102	103	104	28		
(C)	CONSTRUCTION YEAR and API STANDARD	1957	1957	1957	1962		
*(D)	CONSTRUCTION TYPE	W	W	W	W		
(E)	CAPACITY (BBL)	52,170	2,000	2,000	1,010		
(F)	LINING? (Y/N)	Y	Y	N	Y		
(G)	LINING TYPE?						
(H)	TANK HT.(FT)	40	24	24	18		
(I)	MAX. FILL HT. (FT)	36.5	24	24	16.5		
(J)	DIA (FT)	100	25	25	20		
*(K)	ROOF TYPE	EF	F	F	F		
*(L)	VOLUMETRIC ALARM(S)	HH	HH	HH	HH		
(M)	DIKE VOLUME (BBL)	98,170	93,855	88,784	92,090		
*(N)	DATE LAST INTERNAL INSPECTION	6/29/2004	7/11/2003	4/10/2002	8/6/2003		
*(O)	OUT OF SERVICE REPAIR OR OTHER MAJOR REPAIR	1/12/2005 new floor	11/4/2003 new floor	4/18/2002 new floor	8/6/2003 new repair		
(P)	DATE API 653 APPLIED	6/29/2004	7/11/2003	4/10/2002	8/6/2003		
*(Q)	CP TYPE & ANODE TYPE	R	R	R	R		
*(R)	C P MONITORING	Yes	Yes	Yes	Yes		
(S)	DUE DATE FOR NEXT INTERNAL INSPECTION?	6/29/2014	7/11/2013	4/10/2012	8/6/2023		
(T)	INTERNAL INSPECTION INTERVAL? (YEARS)	10 years	10 years	10 years	20 years		
*(U)	INTERNAL INSPECTION INTERVAL BASIS?	New floor	New floor	New floor	M		
(V)	DUE DATE FOR NEXT EXTERNAL INSPECTION?	6/29/2014	7/10/2013	4/10/2012	4/28/2013		
*(W)	EXTERNAL INSPECTION INTERVAL BASIS?	M	M	M	M		
(X)	DUE DATE FOR NEXT U. T. INSPECTION?	6/29/2014	7/10/2013	4/10/2012	4/28/2013		
(Y)	SHELL U.T. INSPECTION INTERVAL	5 years	5 years	5 years	5 years		
*(Z)	SHELL U.T. INSPECTION INTERVAL BASIS?	M	M	M	M		

NOTE: Enter the applicable codes below in the table above:

(A): (R) Refined; (C) Crude; (HVL) Highly Volatile Liquid; (O) Other
(D): (W) Welded; (R) Riveted; (B) Bolted; Note if Tank is Insulated
(K): (EF) External Floater; (IF) Internal Floater; (F) Fixed
(L): (H) High; (HH) High-High; (OF) Overfill; (O) Other
(N): Most Recent Date
(O): Most Recent Date
(Q): (A) Anodic; (R) Rectified (N) None - Document why not needed.
(R): (F) Fixed Reference Cells Under Floor; (S) CP Monitored at Edge of Shell
(U): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service
(W): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service
(Z): (C) Calculation (based upon known corrosion rate); (M) API Maximum Allowed Interval; (O) Other; (SS) Similar Service

Comments:

All breakout tanks are designed to API Standard **650** or its predecessor Standard **12C**.